

BIKE-MSCA-ITN, BImetallic catalysts Knowledgebased development for Energy applications Sofia workshop , 24-26 June, 2020



Synthesis of mesoporous oxides as catalysts or catalytic supports for various redox processes

Assoc. Prof. Dr. Momtchil Dimitrov



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Scheme of the scientific work:





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Scheme of lab work (synthesis part):



Use of post-synthetic modification in order to get the final material







- Why mesoporous oxides?
- Synthesis and characterization of ordered mesoporous silicas
- Introduction of metal/metal oxide active phase within mesoporous silicas
- Metal/metal oxide active phase within ordered mesoporous silicas
- Some applications as catalysts for redox processes
- Synthesis of mesoporous metal oxides
- Introduction of a transition metal/metal oxide component within mesoporous metal oxides
- Multicomponent mesoporous metal oxide systems
- Characterization and application of obtained composites in various redox processes.





Zeolites – well ordered, microporous and crystalline aluminosilicate materials



Main disadvantage: small pore sizes (<< 2 nm) and hence deteriorated transportation + facile coke formation







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 $C_n H_{2n+1} (CH_3)_3 N^+$, (n = 12 – 20)



Synthesis of ordered mesoporous silicas



sol gel process:

1. Aqueous surfactant solution with surfactant concentration above Cmc



- 2. TEOS hydrolysis: Si(OC₂H₅)₄ + H₂O \rightarrow Si(OH)₄ + 4C₂H₅OH; Si(OH)₄ \rightarrow SiO₂ + 2H₂O
- 3. Preferential polymerization of silicate oligomers at the surfactant boundary surface
- 4. Calcination for surfactant removal







 $C_nH_{2n+1}(CH_3)_3N^+$ + source of Si (TEOS) + pH>11

Molecular template process

n=6-10 T=200°C (hydrothermal treatment) high solubility of surfactant molecules

n=12-22 T=100-150°C (HT) low solubility of surfactant molecules

Supramolecular template process

Microporous ZSM-5 zeolite



Ordered mesoporous silica (MCM-41)





Main characteristics from application point of view: 1) type of mesoporous structure;2) pore size and wall thickness and 3) specific surface area and total pore volume





Synthesis of ordered mesoporous silicas



Hydrophilic head Hydrophobic tail Surfactant OH Triton X-100 Non-ionic Surfactant Br Cetyltrimethylammonium Bromide (CTAB) **Cationic Surfactant** 0 0=\$=0 Dioctylsulfosuccinate sodium (AOT) Anionic Surfactant Choline **Zwitterionic Surfactant** Phosphatidylcholine b а



neutral block copolymer surfactant – (PEO)_y-(PPO)_x-(PEO)_y





Pluronic 123 - (PEO)₂₀-(PPO)₇₀-(PEO)₂₀





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Characterization of ordered mesoporous silicas





Characterization of ordered mesoporous silicas

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Application

MTO process (strong acidic sites are needed) Catalysts – zeolites, aluminophosphates



Methanol decomposition

(redox sites are needed) Catalysts – nanosized metals/metal oxides supported on ordered mesoporous silicas





Modification of ordered mesoporous silicas



1) Incipient wetness impregnation with metal nitrates

Advantages:

- easy and fast procedure
- possibility to load the desired amount at one step

Disadvantages:

 lack of good control on the dispersion of the loaded metal phase

2) Impregnation with metal acetylacetonates

Advantages:

fine dispersion of the loaded metal phase

Disadvantages:

- more complicated procedure
- difficult control on the loaded amount













What are the requirements for a supported metal/metal oxide phase within high surface area mesoporous silca in order to possess high and stable catalytic activity for a given redox catalytic reaction?

The supported metal/metal oxide phase should possess the following characteristcs:

- Improved activity favored by its presence in nanosize form thus possessing large active surface available for the reactants (high surface to core ratio)
- Improved redox behavior at low temperatures favored by its improved dispersion and lack of very strong interaction with the support that would deteriorate it.
- High exposure to reactants favored by its homogeneous distribution within an open support mesoporous structure that offers good transportation of reactants and products.
- High stability under reaction conditions favored by its presence within the porous network where its mobility is limited or is in interaction with another component (e.g. another metal) serving as an anchoring site.





Parameters that influence the dispersion and activity of the loaded active metal oxide species within mesoporous silica:

- 1) Support characteristics:
- Type of mesoporous silica structure used as support
- Pore diameter
- Total pore volume
- 2) Supported metal/metal oxide characteristics:
- Type of metal
- Type of the metal precursor
- Content of the loaded metal/metal oxide
- State of supported metal/metal oxide phase
- 3) Procedure of metal/metal oxide loading:
- Modification approach
- Final calcination temperature
- 4) The type of studied catalytic reaction



Metal/metal oxide active phase within ordered mesoporous silicas



• The use of metal acetylacetonate as a precursor in comparison with metal nitrate one leads to the deposition of more finely dispersed metal oxide phase distributed more homogeneously within the ordered mesoprous silica support



Mean diameter, nm

Finely dispersed copper oxide within KIT-6 silica by using copper acetyl acetonate as copper precursor

Presence of large copper oxide particles on the outer surface of KIT-6 silica after impregnation with copper nitrate



Metal/metal oxide active phase within ordered

mesoporous silicas



There is close relation between the reducing ability of the loaded metal oxides and their methanol conversion ability.



- small oligonuclear (FeO)_n species very active at low temperatures (500-650 K)
- bulky clusters of Fe₂O₃ active at ~700K
- isolated Fe³⁺ ions in strong interaction with the support inactive in the studied temperature interval



Metal/metal oxide active phase within ordered

mesoporous silicas



Influence of the content of the supported metal on the catalytic properties in methanol decomposition reaction



- Predominant presence of finely dispersed metal oxides within the MCM-41 pore structure that are very active – this is the case of 8Cu/MCM-41
- Predominant presence of larger (bulk) metal oxide particles on the outer MCM-41 surface – exposed but with low activity due to their low overall reactive surface (low shell/core ratio) – this is the case of 12Cu/MCM-41
- Presence of high amount of isolated metal ions that are in strong interaction with the support silanols – not active but can stabilize finely dispersed metal oxide species in their vicinity – this is the case of 2Cu/MCM-41



Metal/metal oxide active phase within ordered mesoporous silicas



Influence of the supported active phase



- The metallic copper is more active than copper oxide in the reaction
- Above 550 600 K the pre-reduced and oxidized catalysts show close catalytic activity due to unification of the active phase under reaction conditions
- The catalysts obtained by using copper acetylacetonate as copper precursor show higher activity than their analogues obtained by copper nitrate due to higher active phase dispersion



Application



Volatile organic compounds (VOCs) – a major challenge!

Mars-van Krevelen mechanism of VOCs oxidation



For VOC oxidation active sites with improved redox behavior are needed





- Both pure ceria and copper oxide modifications possess large metal oxide particles situated, however the ceria modification is much more active due to the presence of defects in the ceria lattice which favor the reaction.
- The highest activity is registered for the bi-component modification due to presence of only very highly dispersed and X-ray amorphous metal oxide particles within this sample.
- The addition of copper oxide to ceria favors the selectivity of the reaction to total oxidation as the found interaction between copper and ceria decreases the high intrinsic acidity of ceria and even further improves its redox properties.





evaporation induced self-assembly (EISA) approach – ordered mesoporous SnO₂ films and powders

Spin-coating



Drying

spin coated & dried



spin coated & dried DHT



psHT



70/100°C and 70% humidity calcination



400 °C

400 °C







evaporation induced self-assembly (EISA) approach – mesoporous SnO₂ films and powders



SnO₂ films with ordered mesoporous structure



SnO₂ powders with worm-like mesoporous structure



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evaporation induced self-assembly (EISA) approach – nanosized mesoporous SnO₂ powder







Preparation approach



Important characteristics of transition metals + Ce:

- have high reactivity toward hydrolysis and condensation
- possess different oxidation states and coordination
- their oxides tend to crystallize when heated

Very important step – hydrothermal treatment of the solution after the precipitation step: Metal hydroxides are transformed into crystalline oxides – registered by XRD technique









Modification, characterization and application

Preparation approach: comparison of support calcination temperature – 573 K vs 773 K

Sample	Fe,	S _{BET}	V _{tot}	Crystalline phase	D,
	wt. %	m^2/g	cm ³ /g		nm
TiO ₂ -HT-573	-	288	0.31	TiO ₂ (anatase)	8.6
Fe/TiO ₂ -HT-573	12	97	0.22	TiO_2 (anatase)	9.1
TiO ₂ -HT-573	-	90	0.24	α -Fe ₂ O ₃ (hematite) TiO ₂ (anatase)	7.6 16.6
Fe/TiO ₂ -HT-773	12	69	0.18	TiO_2 (anatase) α -Fe ₂ O ₃ (hematite)	14.2 25.2









Synthesis of bicomponent mesoporous metal oxides



Template-assisted precipitation followed by hydrothermal treatment and calcination





Characterization and application









Sample	S _{BET} , m²/g	V _{tot} , cm³/g	Space group	Crystallite size, nm
ZrO ₂ (CTAB, HT373)573	296	0.42	P4 ₂ /nmcZ (tetragonal ZrO ₂)	1.2
1Ce9Zr(CTAB, HT373)573	196	0.16	P4 ₂ /nmcZ	5.1
3Ce7Zr(CTAB, HT373)573	167	0.14	Fm3m (cubic CeO ₂)	3.5
5Ce5Zr(CTAB, HT373)573	150	0.14	Fm3m (44.0 %) P4 ₂ /nmcZ (56.0 %)	8.1 5.4
7Ce3Zr(CTAB, HT373)573	118	0.14	Fm3m (58.4 %) P4 ₂ /nmcZ (41.6 %)	12.8 5.0
9Ce1Zr(CTAB, HT373)573	93	0.20	Fm3m (95.0 %) P4 ₂ /nmcZ (5.0 %)	13.6 4.3
CeO ₂ (CTAB, HT373)573	58	0.27	Fm3m	11.7



500 nn

500 m

Cu/TiO2 WI

Cu/2Ce8Ti WI

Cu/5Ce5Ti WI

Cu/8Ce2Ti WI



Multicomponent metal oxide systems

Support composition	Supports		WI modifications	
TiO	BET m ² g ⁻¹ 85	Vt mlg ⁻¹ 0.29	BET $m^2 g^{-1}$ 40	Vt mlg ⁻¹ 0.24
2Ce8Ti	166	0.62	102	0.49
Ce2Ti	55	0.45	38	0.39
CeO ₂	46	0.26	24	0.20





<u>500 mm</u> Cu/CeO2_W1 <u>500 nm</u>

The catalytic properties of the multicomponent system are determined by the activity of the formed CuO crystallites and the facile electron transfer within the "conjugated" Ti-Ce-Cu redox centres in the interface layer.



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